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Supplementary Release on a Computationally Efficient Thermodynamic Formulation for Liquid Water for Oceanographic Use

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President:

Dr. Daniel G. Friend
Thermophysical Properties Division
National Institute of Standards and Technology
325 Broadway
Boulder, CO, 80305, USA

Executive Secretary:

Dr. R. B. Dooley
Structural Integrity Associates, Inc.
2616 Chelsea Drive
Charlotte, NC 28209, USA
email: bdooley@structint.com

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The equation of state provided in this release is a fundamental equation for the Gibbs energy as a function of temperature and pressure; details can be found in the articles “A new extended Gibbs thermodynamic potential of seawater” and “A Gibbs function for seawater thermodynamics for -6 to 80 °C and salinity up to 120 g kg⁻¹” by R. Feistel [1, 2]. This equation can be used instead of the IAPWS-95 formulation [3, 4] for thermodynamic properties of liquid water required for calculating properties of seawater according to the IAPWS seawater formulation [5]. It is restricted to the oceanographic standard range of temperature and pressure, within which its deviations from IAPWS-95 are well within the uncertainties of IAPWS-95.

Further information about this supplementary release and other documents issued by IAPWS can be obtained from the Executive Secretary of IAPWS or from <http://www.iapws.org>.

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1 Nomenclature

Symbol	Physical quantity	Unit
c_p	Specific isobaric heat capacity	$\text{J kg}^{-1} \text{K}^{-1}$
h	Specific Helmholtz energy	J kg^{-1}
g	Specific Gibbs energy	J kg^{-1}
g^*	Reducing specific Gibbs energy, $g^* = 1 \text{ J kg}^{-1}$	J kg^{-1}
$g_{00} \dots g_{76}$	Coefficients of the Gibbs potential function, Table 2	
h	Specific enthalpy	J kg^{-1}
k	Uncertainty coverage factor	
p	Absolute pressure	Pa
p_0	Normal pressure, $p_0 = 101\,325 \text{ Pa}$	Pa
p_t	IAPWS-95 calculated triple-point pressure, $p_t = 611.654\,771\,007\,894 \text{ Pa}$	Pa
p^*	Reducing pressure, $p^* = 10^8 \text{ Pa}$	Pa
s	Specific entropy	$\text{J kg}^{-1} \text{K}^{-1}$
T	Absolute temperature (ITS-90)	K
T_0	Celsius zero point, $T_0 = 273.15 \text{ K}$	K
T_t	Triple-point temperature, $T_t = 273.16 \text{ K}$	K
T^*	Reducing temperature, $T^* = 40 \text{ K}$	K
t	Celsius temperature	$^{\circ}\text{C}$
t_{\min}	Lower temperature bound	$^{\circ}\text{C}$
u	Specific internal energy	J kg^{-1}
U	Expanded uncertainty	
u_c	Combined standard uncertainty	

Symbol	Physical quantity	Unit
v	Specific volume	$\text{m}^3 \text{kg}^{-1}$
w	Speed of sound	m s^{-1}
α	Thermal expansion coefficient	K^{-1}
β_s	Isentropic temperature-pressure coefficient	K Pa^{-1}
κ_s	Isentropic compressibility	Pa^{-1}
κ_T	Isothermal compressibility	Pa^{-1}
π	Reduced pressure, $\pi = (p - p_0) / p^*$	
ρ	Density	kg m^{-3}
τ	Reduced temperature, $\tau = (T - T_0) / T^*$	

2 Introductory Remarks and Special Constants

The “Release on the IAPWS Formulation 2008 for the Thermodynamic Properties of Seawater” [5] describes the difference between the specific Gibbs energies of seawater and water. At given temperature and pressure, the water part must separately be computed from the Helmholtz function provided by the IAPWS-95 formulation [3, 4], determining the pure-water density by numerical iteration. As a function of temperature and pressure, the Gibbs function for liquid water provided in this Supplementary Release eliminates the need for iteration. It is restricted in its validity to the range 100 Pa to 100 MPa and $t_{\min}(p) = -(2.65 + p \times 0.0743 \text{ MPa}^{-1})^\circ\text{C}$ to 40°C , only slightly exceeding the oceanographic standard range to include the triple point and the lowest oceanic freezing point. This Gibbs function significantly simplifies the implementation and reduces the computing time for oceanographic applications such as numerical circulation models or real-time processing of in-situ data, while still giving values for properties whose agreement with IAPWS-95 is well within the uncertainties associated with IAPWS-95.

TABLE 1 Special constants and values used in this release

Quantity	Symbol	Value	Unit	Reference
Triple-point pressure ^a	p_t	611.654 771 007 894	Pa	[3]
Normal pressure	p_0	101 325	Pa	[7]
Reducing pressure	p^*	10^8	Pa	[2]
Triple-point temperature	T_t	273.16	K	[8]
Celsius zero point	T_0	273.15	K	[8]
Reducing temperature	T^*	40	K	[2]

^aNumerical triple-point pressure value computed from IAPWS-95 [3], being well within the uncertainty of the experimental value of 611.657(10) Pa [6]

3 The Equation of State

The equation of state presented here is in the form of the specific Gibbs energy as a function of temperature and pressure, $g(T, p)$, corresponding to a Gibbs potential. The temperatures are based on the temperature scale ITS-90 [8]. Reduced by $g^* = 1 \text{ J kg}^{-1}$, the Gibbs function is the dimensionless polynomial given by Eq. (1)

$$g(T, p)/g^* = \sum_{j=0}^7 \sum_{k=0}^6 g_{jk} \tau^j \pi^k, \quad (1)$$

with the reduced temperature $\tau = (T - T_0)/T^*$ and the reduced pressure $\pi = (p - p_0)/p^*$. The reduced quantities τ and π vary from 0 to 1 in the oceanographic standard range. The constants T_0, p_0, T^* , and p^* are given in Table 1.

The coefficients of Eq. (1) are given in Table 2. Two of these 41 parameters (g_{00} and g_{10}) are arbitrary and are computed from the reference-state conditions of vanishing specific entropy, s , and specific internal energy, u , of liquid water at the triple point,

$$s(T_t, p_t) = 0, \quad (2)$$

$$u(T_t, p_t) = 0. \quad (3)$$

TABLE 2 Coefficients of the Gibbs function, as given by Eq. (1). Coefficients not contained in this table have the value $g_{jk} = 0$.

j	k	g_{jk}	j	k	g_{jk}
0	0	0.101 342 743 139 674 $\times 10^3$	3	2	0.499 360 390 819 152 $\times 10^3$
0	1	0.100 015 695 367 145 $\times 10^6$	3	3	-0.239 545 330 654 412 $\times 10^3$
0	2	-0.254 457 654 203 630 $\times 10^4$	3	4	0.488 012 518 593 872 $\times 10^2$
0	3	0.284 517 778 446 287 $\times 10^3$	3	5	-0.166 307 106 208 905 $\times 10$
0	4	-0.333 146 754 253 611 $\times 10^2$	4	0	-0.148 185 936 433 658 $\times 10^3$
0	5	0.420 263 108 803 084 $\times 10$	4	1	0.397 968 445 406 972 $\times 10^3$
0	6	-0.546 428 511 471 039	4	2	-0.301 815 380 621 876 $\times 10^3$
1	0	0.590 578 347 909 402 $\times 10$	4	3	0.152 196 371 733 841 $\times 10^3$
1	1	-0.270 983 805 184 062 $\times 10^3$	4	4	-0.263 748 377 232 802 $\times 10^2$
1	2	0.776 153 611 613 101 $\times 10^3$	5	0	0.580 259 125 842 571 $\times 10^2$
1	3	-0.196 512 550 881 220 $\times 10^3$	5	1	-0.194 618 310 617 595 $\times 10^3$
1	4	0.289 796 526 294 175 $\times 10^2$	5	2	0.120 520 654 902 025 $\times 10^3$
1	5	-0.213 290 083 518 327 $\times 10$	5	3	-0.552 723 052 340 152 $\times 10^2$
2	0	-0.123 577 859 330 390 $\times 10^5$	5	4	0.648 190 668 077 221 $\times 10$
2	1	0.145 503 645 404 680 $\times 10^4$	6	0	-0.189 843 846 514 172 $\times 10^2$
2	2	-0.756 558 385 769 359 $\times 10^3$	6	1	0.635 113 936 641 785 $\times 10^2$
2	3	0.273 479 662 323 528 $\times 10^3$	6	2	-0.222 897 317 140 459 $\times 10^2$
2	4	-0.555 604 063 817 218 $\times 10^2$	6	3	0.817 060 541 818 112 $\times 10$
2	5	0.434 420 671 917 197 $\times 10$	7	0	0.305 081 646 487 967 $\times 10$
3	0	0.736 741 204 151 612 $\times 10^3$	7	1	-0.963 108 119 393 062 $\times 10$
3	1	-0.672 507 783 145 070 $\times 10^3$			

TABLE 3 Relations of the thermodynamic properties to the equation for the Gibbs energy of liquid water, Eq. (1), and its T - p derivatives^a

Property	Relation	Unit	Eq.
Density			
$\rho(T, p) = v^{-1} = (\partial g / \partial p)_T^{-1}$	$\rho(T, p) = g_p^{-1}$	$\frac{\text{kg}}{\text{m}^3}$	(4)
Specific entropy			
$s(T, p) = -(\partial g / \partial T)_p$	$s(T, p) = -g_T$	$\frac{\text{J}}{\text{kg K}}$	(5)
Specific isobaric heat capacity			
$c_p(T, p) = T(\partial s / \partial T)_p$	$c_p(T, p) = -T g_{TT}$	$\frac{\text{J}}{\text{kg K}}$	(6)
Specific enthalpy			
$h(T, p) = g + Ts$	$h(T, p) = g - T g_T$	$\frac{\text{J}}{\text{kg}}$	(7)
Specific internal energy			
$u(T, p) = g + Ts - pv$	$u(T, p) = g - T g_T - p g_p$	$\frac{\text{J}}{\text{kg}}$	(8)
Specific Helmholtz energy			
$f(T, p) = g - pv$	$f(T, p) = g - p g_p$	$\frac{\text{J}}{\text{kg}}$	(9)
Thermal expansion coefficient			
$\alpha(T, p) = v^{-1}(\partial v / \partial T)_p$	$\alpha(T, p) = g_{Tp} / g_p$	$\frac{1}{\text{K}}$	(10)
Isentropic temperature-pressure coefficient, adiabatic lapse rate			
$\beta_s(T, p) = (\partial T / \partial p)_s$	$\beta_s(T, p) = -g_{Tp} / g_{TT}$	$\frac{\text{K}}{\text{Pa}}$	(11)
Isothermal compressibility			
$\kappa_T(T, p) = -v^{-1}(\partial v / \partial p)_T$	$\kappa_T(T, p) = -g_{pp} / g_p$	$\frac{1}{\text{Pa}}$	(12)
Isentropic compressibility			
$\kappa_s(T, p) = -v^{-1}(\partial v / \partial p)_s$	$\kappa_s(T, p) = (g_{Tp}^2 - g_{TT} g_{pp}) / (g_p g_{TT})$	$\frac{1}{\text{Pa}}$	(13)
Speed of sound			
$w(t, p) = \sqrt{(\partial p / \partial \rho)_s}$	$w(T, p) = g_p \sqrt{g_{TT} / (g_{Tp}^2 - g_{TT} g_{pp})}$	$\frac{\text{m}}{\text{s}}$	(14)

^a $g_T \equiv \left[\frac{\partial g}{\partial T} \right]_p$, $g_p \equiv \left[\frac{\partial g}{\partial p} \right]_T$, $g_{TT} \equiv \left[\frac{\partial^2 g}{\partial T^2} \right]_p$, $g_{Tp} \equiv \frac{\partial^2 g}{\partial T \partial p}$, $g_{pp} \equiv \left[\frac{\partial^2 g}{\partial p^2} \right]_T$

4 Relations of the Thermodynamic Properties to the Specific Gibbs Energy

Thermodynamic properties can be derived from Eq. (1) by using the appropriate combinations of the specific Gibbs energy and its derivatives. Relations between thermodynamic properties and $g(T, p)$ and its derivatives with respect to T and p are summarized in Table 3. All required derivatives of the saline part of the specific Gibbs energy are explicitly given in Table 4.

TABLE 4 Equations for the Gibbs energy, Eq. (1), and its derivatives^a

Equation	Unit
$g(T, p) = g^* \sum_{j=0}^7 \sum_{k=0}^6 g_{jk} \tau^j \pi^k$ <p>with $g^* = 1 \text{ J kg}^{-1}$,</p> $\tau = (T - T_0)/T^*, \quad T_0 = 273.15 \text{ K}, \quad T^* = 40 \text{ K},$ $\pi = (p - p_0)/p^*, \quad p_0 = 101325 \text{ Pa}, \quad p^* = 10^8 \text{ Pa}$	$\frac{\text{J}}{\text{kg}}$
$g_T(T, p) = \frac{g^*}{T^*} \sum_{j=1}^7 \sum_{k=0}^6 j g_{jk} \tau^{j-1} \pi^k$	$\frac{\text{J}}{\text{kg K}}$
$g_p(T, p) = \frac{g^*}{p^*} \sum_{j=0}^7 \sum_{k=1}^6 k g_{jk} \tau^j \pi^{k-1}$	$\frac{\text{m}^3}{\text{kg}}$
$g_{TT}(T, p) = \frac{g^*}{(T^*)^2} \sum_{j=2}^7 \sum_{k=0}^6 j(j-1) g_{jk} \tau^{j-2} \pi^k$	$\frac{\text{J}}{\text{kg K}^2}$
$g_{Tp}(T, p) = \frac{g^*}{T^* p^*} \sum_{j=1}^7 \sum_{k=1}^6 jk g_{jk} \tau^{j-1} \pi^{k-1}$	$\frac{\text{m}^3}{\text{kg K}}$
$g_{pp}(T, p) = \frac{g^*}{(p^*)^2} \sum_{j=0}^7 \sum_{k=2}^6 k(k-1) g_{jk} \tau^j \pi^{k-2}$	$\frac{\text{m}^3}{\text{kg Pa}}$
$^a g_T \equiv \left[\frac{\partial g}{\partial T} \right]_p, \quad g_p \equiv \left[\frac{\partial g}{\partial p} \right]_T, \quad g_{TT} \equiv \left[\frac{\partial^2 g}{\partial T^2} \right]_p, \quad g_{Tp} \equiv \frac{\partial^2 g}{\partial T \partial p}, \quad g_{pp} \equiv \left[\frac{\partial^2 g}{\partial p^2} \right]_T$	

5 Range of Validity and Brief Discussion

The equation of state, Eq. (1), is valid for liquid water only within the pressure and temperature range

$$100 \text{ Pa} \leq p \leq 10^8 \text{ Pa} \text{ and } (270.5 - p \times 7.43 \times 10^{-8} \text{ Pa}^{-1}) \text{ K} \leq T \leq 313.15 \text{ K},$$

including the region of ambient ocean water. The lower temperature limit depends on the pressure proportional to the experimental Clausius-Clapeyron coefficient [9] and covers the lowest temperature found in the global ocean: the freezing temperature of about $-4.25 \text{ }^\circ\text{C}$ off the Antarctic shelf at 3000 m depth. The deviations of properties derived from this Gibbs function from those calculated with IAPWS-95 are significantly less than the experimental uncertainty for each property (Table 5). Within its range of validity, it is intended to be used as a simpler substitute for IAPWS-95, providing the water part of the Gibbs function of seawater [5] without significant loss in accuracy.

This formulation for the thermodynamic properties of liquid water was developed in cooperation with the SCOR/IAPSO Working Group 127 on Thermodynamics and Equation of State of Seawater.

6 Estimates of Uncertainty

Here, estimated combined standard uncertainties u_c [10] are reported, from which expanded uncertainties $U = k u_c$ can be obtained by multiplying with the coverage factor $k = 2$, corresponding to a 95% confidence level. The term ‘‘uncertainty’’ used in the following refers to combined standard uncertainties or to relative combined standard uncertainties.

Deviations of selected properties of this supplementary release from IAPWS-95 are reported in Table 5. These deviations are well within the estimated uncertainties of IAPWS-95.

TABLE 5 Combined standard uncertainties from IAPWS-95 [3, 4] of selected quantities in certain regions of the T - p space, compared with the root-mean-square (r.m.s.) and the maximum deviation between IAPWS-95 and the formulation of this release. The pressure-dependent lower temperature bound is $t_{\min} = -(2.65 + p \times 0.0743 \text{ MPa}^{-1}) \text{ }^\circ\text{C}$. For ρ and w the uncertainties and deviations are relative and therefore dimensionless.

Quantity	T interval $^\circ\text{C}$	p interval MPa	IAPWS-95 Uncertainty	r.m.s. Deviation	Maximum Deviation	Units
c_p	-2.7 - 40	0.1	10	0.04	0.25	$\text{J kg}^{-1} \text{ K}^{-1}$
α	-2.7 - 40	0.1	0.6×10^{-6} ^a	0.03×10^{-6}	0.19×10^{-6}	K^{-1}
α	$t_{\min}(p)$ - 40	0.0001 - 100	0.6×10^{-6} ^a	0.02×10^{-6}	0.19×10^{-6}	K^{-1}
ρ	-2.7 - 40	0.1	1×10^{-6}	0.03×10^{-6}	0.23×10^{-6}	–
ρ	$t_{\min}(p)$ - 40	0.0001 - 10	10×10^{-6}	0.03×10^{-6}	0.23×10^{-6}	–
ρ	$t_{\min}(p)$ - 40	10 - 100	30×10^{-6}	0.04×10^{-6}	0.23×10^{-6}	–
w	$t_{\min}(p)$ - 40	0.0001 - 100	1000×10^{-6}	3×10^{-6}	39×10^{-6}	–

^a Estimate adopted from seawater data [1]

7 Computer-Program Verification

To assist the user in computer-program verification, Table 6 with test values is given. It contains values for the specific Gibbs energy, $g(T, p)$, together with the corresponding derivatives and some thermodynamic properties.

8 References

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TABLE 6 Numerical check values for the Gibbs function g and its derivatives, Table 4, The numerical functions evaluated here at given points (T, p) are defined in Tables 3 and 4.

Quantity	Value	Value	Value	Unit
T	273.15	273.15	313.15	K
p	101 325	10^8	101 325	Pa
g	$0.101\ 342\ 743 \times 10^3$	$0.977\ 303\ 868 \times 10^5$	$-0.116\ 198\ 898 \times 10^5$	J kg^{-1}
$(\partial g/\partial T)_p$	0.147 644 587	$0.851\ 506\ 346 \times 10$	$-0.572\ 365\ 181 \times 10^3$	$\text{J kg}^{-1} \text{K}^{-1}$
$(\partial g/\partial p)_T$	$0.100\ 015\ 695 \times 10^{-2}$	$0.956\ 683\ 354 \times 10^{-3}$	$0.100\ 784\ 471 \times 10^{-2}$	$\text{m}^3 \text{kg}^{-1}$
$(\partial^2 g/\partial T^2)_p$	$-0.154\ 472\ 324 \times 10^2$	$-0.142\ 970\ 174 \times 10^2$	$-0.133\ 463\ 968 \times 10^2$	$\text{J kg}^{-1} \text{K}^{-2}$
$\partial^2 g/\partial T \partial p$	$-0.677\ 459\ 513 \times 10^{-7}$	$0.199\ 088\ 060 \times 10^{-6}$	$0.388\ 499\ 694 \times 10^{-6}$	$\text{m}^3 \text{kg}^{-1} \text{K}^{-1}$
$(\partial^2 g/\partial p^2)_T$	$-0.508\ 915\ 308 \times 10^{-12}$	$-0.371\ 527\ 164 \times 10^{-12}$	$-0.445\ 841\ 077 \times 10^{-12}$	$\text{m}^3 \text{kg}^{-1} \text{Pa}^{-1}$
h	$0.610\ 136\ 242 \times 10^2$	$0.954\ 044\ 973 \times 10^5$	$0.167\ 616\ 267 \times 10^6$	J kg^{-1}
f	$0.183\ 980\ 891 \times 10^{-2}$	$0.206\ 205\ 140 \times 10^4$	$-0.117\ 220\ 097 \times 10^5$	J kg^{-1}
u	$-0.403\ 272\ 791 \times 10^2$	$-0.263\ 838\ 183 \times 10^3$	$0.167\ 514\ 147 \times 10^6$	J kg^{-1}
s	-0.147 644 587	$-0.851\ 506\ 346 \times 10$	$0.572\ 365\ 181 \times 10^3$	$\text{J kg}^{-1} \text{K}^{-1}$
ρ	$0.999\ 843\ 071 \times 10^3$	$0.104\ 527\ 793 \times 10^4$	$0.992\ 216\ 354 \times 10^3$	kg m^{-3}
c_p	$0.421\ 941\ 153 \times 10^4$	$0.390\ 523\ 030 \times 10^4$	$0.417\ 942\ 416 \times 10^4$	$\text{J kg}^{-1} \text{K}^{-1}$
w	$0.140\ 240\ 099 \times 10^4$	$0.157\ 543\ 089 \times 10^4$	$0.152\ 891\ 242 \times 10^4$	m s^{-1}